

# **GESTRA Steam Systems**

Control Valve
With Radial Stage Nozzle ZK and Tandem Shut-Off
ZK 213
DN 80 – 250

Product Range A4

**ZK 213** 

#### **Description**

Control valve for operation at very high differential pressures

Application, for example, in industrial plants and power stations as

- Leak-off valve for condensate pumps etc.
- Injection-cooling valve
- Start-up pot drain valve
- Feedwater control valve

The pressure drop is decreased in the radial stage nozzle ZK in several stages, so that the flow velocity is reduced leading to a considerable reduction in wear and noise (sound level  $\leq$  85 dB(A)).

The dual (tandem) shut-off combines the function of a conventional shut-off valve and a valve provided with regulating cone. At the beginning of the opening process first the main valve plug is lifted off the main seat, while the secondary valve plug remains closed until the main plug has reached a certain lift. At the moment of closing and at the beginning of opening the flow velocity at the valve seat is therefore zero so that wire drawing is exluced.

Angle-type or Z-type valve body.

The valve permits the use of several actuator types:

- 1. ZK 213-.../13 Electric linear actuator
- ZK 213-.../14
   Design with insert bush for fitting an electric rotary actuator or a handwheel
- 3. ZK 213-.../20 Pneumatic diaphragm actuator
- 4. ZK 213-.../40

Hydraulic linear actuator **Example:** ZK 213-E2/14

E = angle version (Z = Z-type version)

2 = size

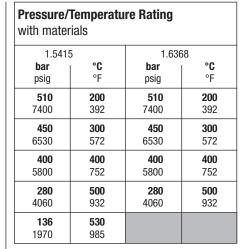
see table "k<sub>vs</sub>-value"

14 = type of actuator

(13, 14, 20, 40)

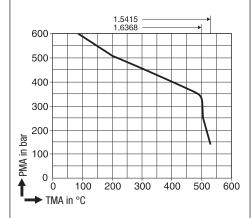
Internals completely exchangeable (incl. seat).

Leak rate acc. to DIN 3230 BN 1.



Differential pressure

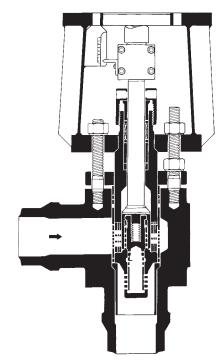
 $\Delta$ PMX 300 bar (4350 psi) – 4 stages 560 bar (8120 psi) – 6 stages



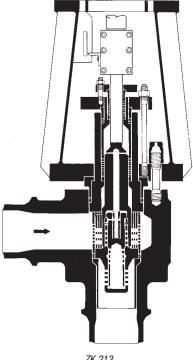
| Materials        |   |
|------------------|---|
| Body             | Forged alloy steel<br>15 Mo3 (1.5415)<br>or WB 36 (1.6368)                            |
| Internals        | s.s. X 35CrMo 17 (1.4122)<br>s.s. X90CrMoV 18 (1.4112)<br>s.s. X20CrMoV 12 1 (1.4922) |
| Gland<br>packing | Pure graphite   |

#### **Connections**

Butt-weld ends. Dimensions on request.

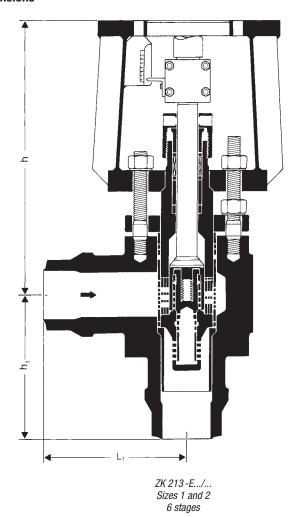


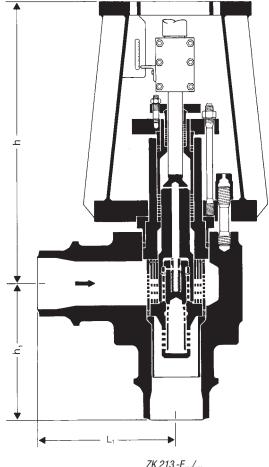
ZK 213 Sizes 1 and 2



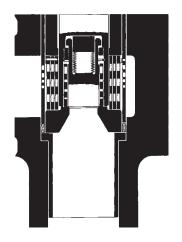
ZK 213 Sizes 3 and 4, partially balanced

## **Dimensions**





ZK 213 -E.../... Sizes 3 and 4 6 stages, partially balanced



ZK 213 4 stages

| Size           | 1                             | 2                             | 3                             | 4                 |
|----------------|-------------------------------|-------------------------------|-------------------------------|-------------------|
| DN mm (in)     | 180 (3)<br>100 (4)<br>125 (5) | 100 (4)<br>125 (5)<br>150 (6) | 125 (5)<br>150 (6)<br>200 (8) | 150<br>200<br>250 |
| h              | 635                           | 735                           | 890                           | 910               |
| h <sub>1</sub> | 260                           | 350                           | 400                           | 400               |
| L <sub>1</sub> | 260                           | 350                           | 400                           | 400               |
| Weight<br>[kg] | 210                           | 370                           | 540                           | 600               |

### Calculation of required k<sub>v</sub> value\*)

- 1. For water flowrates within temperature ranges where flashing because of pressure drop is not to be expected (e.g. leak-off and injection-cooling valves) the calculated  $k_{\nu}$  value has to be multiplied by a correction factor taken from the chart below due to the successive expansion. The chart includes a safety factor of 1.2.
- 2. If, due to the pressure drop, flashing is to be expected, the formulae below should not be used to calculate the  $k_{\nu}$  value. In this case see overleaf for hot water capacity charts. If  $p_2/p_1 > 0.5$  multiply the chart reading by the correction factor K taken from the back pressure chart below. The safety factor of 1.2 must always be taken into consideration.
- 3. For steam the calculated  $k_{\nu}$  value has to be multiplied by a safety factor of 1.2.

| Pressure<br>drop  | <i>k</i> <sub>v</sub> | for li  | quids   | for gas,<br>temperature-corrected  | for vapours  | for saturated<br>and wet steam                            |
|---|-----------------------|---|---|--|--|---|
| $\Delta p < \frac{p_1}{2}$ $\left(p_2 > \frac{p_1}{2}\right)$ | k <sub>v</sub>        | ÿ <b>1</b> /ρ1                                | _ ṁ   | $=\frac{\dot{V}_{N}}{514}\sqrt{\frac{\rho_{N}\cdot T_{1}}{\Delta p\cdot p_{2}}}$ | $=\frac{\dot{m}}{31.6} \sqrt{\frac{v}{\Delta p}}$      | $=\frac{\dot{m}}{31.6} \sqrt{\frac{v \cdot x}{\Delta p}}$ |
| $\Delta p > \frac{p_1}{2}$ $\left(p_2 < \frac{p_1}{2}\right)$ | k <sub>v</sub>        | $=\frac{1}{31.6}$ $\sqrt{\frac{1}{\Delta p}}$ | $= \frac{1}{31.6 \sqrt{\rho_1 \cdot \Delta p}}$ | $= \frac{2\dot{V}_N}{514 \cdot \rho_1} \sqrt{\rho_N \cdot T_1}$                  | $=\frac{\dot{m}}{31.6} \sqrt{\frac{2 \text{ V}}{p_1}}$ | $=\frac{\dot{m}}{31.6} \sqrt{\frac{v\cdotx\cdot2}{p_1}}$  |

<sup>\*)</sup> Conversion Factors:  $C_v$  (U.S.) = 1.17 ·  $k_v$   $C_v$  (U.K.) = 0.98 ·  $k_v$ 

| $k_{v}$ | Value flow coefficient for |  |
|---------|----------------------------|--|
|         | fully open valve within    |  |

Nomenclature:

fully open valve within control range

V Flowrate [m³/h]

m Flowrate [kg/h]

V<sub>N</sub> Volume flowrate for gases at standard state (0°C, 1013 mbar)

(0 °C, 1013 mbar) [m³/h]

 $p_1$  Upstream pressure [bar a]  $p_2$  Downstream pressure [bar a]

 $\Delta p$  Pressure drop  $p_1 - p_2$  [bar]

 $ho_1$  Density of fluid with operating condition at  $T_1$  and  $p_2$  [kg/m³]

 $\rho_{\text{N}}$  Density of gases at standard state (0 °C, 1013 mbar)  $[\text{kg/m}^3]$ 

Specific steam volume at  $T_1$  and  $p_2$  or – if

 $\Delta p > \frac{p_1}{2} - \text{ at } \frac{p_1}{2}$  [m<sup>3</sup>/kg]

[K]

T<sub>1</sub> Absolute inlet temperature of fluid

Content of dry saturated steam in wet steam  $(0 < x \le 1)$ 

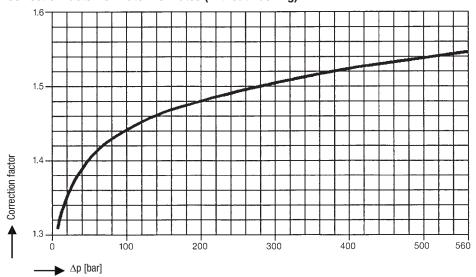
## K<sub>v</sub> Values at Control Stroke H<sub>100</sub>

See page 4: The characteristic lines in the upper part of the chart indicate simultaneously the  $k_{\nu}$  values.

[m3/h]

|          |                        | k <sub>v</sub> values [m³/h]                        |   | Control                         |  |
|----------|------------------------|---|---|---------------------------------|--|
|          | DN                     | 4 stages<br>∆p <sub>max</sub> 300 bar<br>(4350 psi) | 6 stages<br>∆p <sub>max</sub> 560 bar<br>(8120 psi) | stroke<br>H <sub>100</sub> [mm] |  |
| ZK 2131/ | 80 – 125 mm (3 – 5")   | 13  | 10  | 50                              |  |
| ZK 2132/ | 100 – 150 mm (4 – 6")  | 26  | 20  | 60                              |  |
| ZK 2133/ | 125 – 200 mm (5 – 8")  | 39  | 30  | 70                              |  |
| ZK 2134/ | 150 – 250 mm (6 – 10") | 60  | 46  | 70                              |  |

#### **Correction factor for water flowrates (without flashing)**



## Control Valve With Radial Stage Nozzle ZK and Tandem Shut-Off

**ZK 213** DN 80 - 250

#### **Order and Enquiry Specifications**

Control valve with radial stage nozzle ZK and tandem shut-off ZK 213.

Design data: p = ... bar t = ...°C Operational data: Load Conditions (1 - 3)

|                             | 1 | 2 | 3 |
|-----------------------------|---|---|---|
| <i>p</i> <sub>1</sub> [bar] |   |   |   |
| t <sub>1</sub> [°C]         |   |   |   |
| <i>p</i> <sub>2</sub> [bar] |   |   |   |
| ∆p [bar]                    |   |   |   |
| ṁ [t/h]                     |   |   |   |

Please enter data in this table

Fluid: Actuators:

Electric (make)

On-off or modulating control

Voltage/Hz.../... Control voltage/Hz.../...

for electro-hydraulic linear actuators indicate on-off or modulating control ∆p max in bar for sizing of

actuator

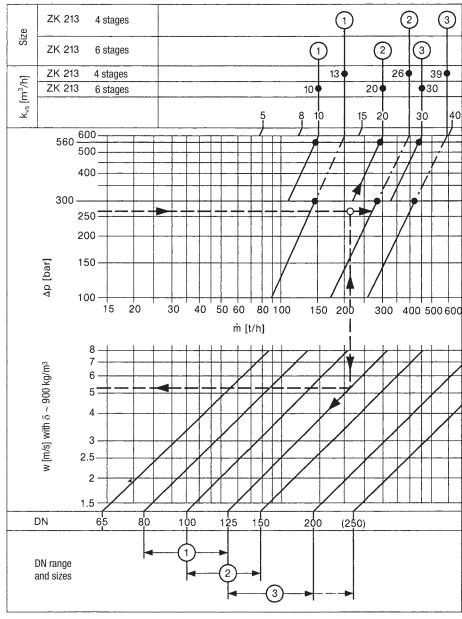
The following test certificates can be issued on request, at extra cost:

In accordance with EN 10204/-2.1, -2.2, -3.1A, -3.1B and -3.1C.

All inspection requirements have to be stated with the order. After supply of the equipment certificates can no longer be established. Charges and extent of the above mentioned certificates as well as the different tests confirmed therein are listed in our leaflet "Test and Inspection Charges for Standard Equipment". For other tests and inspections than those listed above, please consult us.

#### Leak-off valves ZK 213

Chart for determination of size, nominal size and flow velocity v in the pipe



Example: Sizing of a leak-off valve.

Operating conditions:

Upstream pressure  $p_1 = 285$  bar Feedwater temperature t = 210 °C

Back pressure  $p_2 = 15 \text{ bar}$ Flowrate  $\dot{m} = 210 \text{ t/h}$ 

Differential pressure across the leak-off valve  $\Delta p = 270$  bar (upstream pressure minus back pressure)

In accordance with the above chart, the required  $k_{\nu}$  value for a flowrate of 210 t/h is 20 m<sup>3</sup>/h.

Since the differential pressure  $\Delta p$  is lower than 300 bar, the ZK 213 with 4 stages, size 2, with a  $k_v$  value of 26 m<sup>3</sup>/h

For each valve size 3 different nominal sizes are available;

for size 2 these are DN 100, 125 and 150 (4, 5 and 6").

For leak-off lines we recommend flow velocities between 4 and 8 m/s.

From the lower part of the chart indicating the flow velocities we can read a velocity of 5.4 m/s for DN 125, i.e. DN 125 mm should be selected.

Supply in accordance with our general terms of business.

P. O. Box 10 54 60. D-28054 Bremen Münchener Str. 77, D-28215 Bremen

Telephone +49 (0) 421 35 03 - 0, Fax +49 (0) 421 35 03-393

E-Mail gestra.ag@flowserve.com, Internet www.gestra.de

